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(54) Title: PROCESS FOR PREPARING PIGMENTS DISPERSIBLE IN PAINTS AND PLASTICS CONCENTRATES

(57) Abstract: A process for preparing an improved pigment which is readily dispersible in paints and plastics concentrates is provided. In accordance with the process, a particulate pigment is mixed with water to form a slurry thereof, and a surface active agent is mixed with the slurry so that the pigment therein is coated therewith. A preferred surface active agent is a mixture of ethoxylated sorbitan derivatives, non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides. After the pigment has been coated with the surface active agent, the coated pigment is dried.

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PROCESS FOR PREPARING PIGMENTS DISPERSIBLE IN PAINTS AND PLASTICS CONCENTRATES

5 The present invention relates to a process for preparing an improved inorganic pigment having enhanced dispersibility in paints and plastics concentrates as determined by the time or energy required to achieve dispersal.

10 Inorganic pigments such as titanium dioxide, zinc sulfide, zinc oxide and the like are used in paint, plastics and other products. Such pigments have heretofore been difficult to disperse in paints and plastics concentrates, that is, the pigments have required long time periods and/or high levels of energy to achieve dispersal. Inorganic pigments are generally in the form of a finely divided powder which has been jet-milled or micronized as a final step in their production.

15 More recently, processes have been developed and used for preparing low-dusting, free-flowing pigment which requires less energy to disperse in paints and plastics concentrates. For example, U.S. Patent No. 5,733,365 and related U.S. Patent No. 5,908,498 disclose a process for preparing improved low-dusting, free-flowing pigments which have not been subjected to final micronizing treatments. The process is comprised of the steps of providing an inorganic pigment material which has not
20 been micronized, providing a source of water, forming a fine, well dispersed slurry of the pigment and water, milling the slurry, adjusting the pH of the slurry, depositing a treating agent having the formula $\text{ROOCCHSO}_3\text{MCH}_2\text{COOR}'$ wherein R and R' are monovalent alkyl radicals having from about 2 to about 20 carbon atoms and M is a metallic monovalent cation on the slurried milled pigment, and then drying the pigment
25 material having the treating agent deposited thereon. The presence of the treating agent makes the pigment produced more readily dispersible in paints and plastics concentrates.

30 While the pigments produced in accordance with the teachings of the above described patents constitute a major improvement as compared to prior pigments, the dispersal of the pigments in paints and plastics concentrates still requires considerable mixing time, energy and expense.

 Thus, there is a continuing need for a process for preparing improved pigments which are more easily dispersed in paints and plastics concentrates. The present

invention meets this need in providing a process for preparing improved pigment which is more readily dispersible in paints and plastics concentrates, which process comprises the steps of: (a) mixing a particulate pigment with water to form a slurry of the pigment and water; (b) mixing a surface active agent with the slurry of step (a) so that the pigment is coated therewith, the surface active agent being selected from the group consisting of alkyl alcohols ethoxylated with from 4 to 14 ethylene oxide groups and wherein the alkyl groups have from 6 to 16 carbon atoms, ethoxylated sorbitan derivatives having HLB values in the range of from 1 to 20, a mixture of non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides having HLB values in the range of from 1 to 20 and mixtures of said ethoxylated sorbitan derivatives, said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides; and (c) drying the pigment coated in accordance with step (b).

Another process of this invention for preparing improved pigment which is highly dispersible in paints and plastics concentrates comprises the steps of: (a) mixing a particulate pigment with water to form a slurry of the pigment and water; (b) milling the slurry formed in step (a) to produce an average pigment particle size in the range of from 0.1 microns to 1 micron; (c) mixing a surface active agent with the slurry of step (b) so that said pigment is coated therewith, said surface active agent being selected from the group described above; and (d) drying the pigment coated in accordance with step (c).

As mentioned, it has heretofore been difficult to disperse particulate pigments in paints and plastics concentrates or melts. The pigments utilized in paints and plastics concentrates and to which the present invention may therefore be applied include, but are not limited to, white opacifying pigments such as titanium dioxide, basic carbonate white lead, basic sulfate white lead, basic silicate white lead, zinc sulfide, zinc oxide, composite pigments of zinc sulfide and barium sulfate, antimony oxide and the like, white extender pigments such as calcium carbonate, calcium sulfate, china and kaolin clays, mica, diatomaceous earth and colored pigments such as iron oxide, lead oxide, cadmium sulfide, cadmium selenide, lead chromate, zinc chromate, nickel titanate, chromium oxide and the like. The present invention is considered of particular value for improving the dispersibility of the inorganic pigments, however, with titanium dioxide being the most preferred pigment to which the present invention is to be applied.

The pigments produced by the present invention are more readily dispersed in paints and plastics concentrates and require less time and/or energy to disperse than prior art pigments. The treated pigments produced by this invention can be low-dusting and free-flowing non-micronized pigments or the treated pigments can optionally be micronized.

The process of the present invention for preparing improved pigment which is more readily dispersible in paints and plastics concentrates is again basically comprised of the following steps: (a) mixing a particulate pigment with water to form a slurry of the pigment and water; (b) mixing a surface active agent with the slurry of step (a) so that the pigment is coated therewith; and (c) drying the pigment coated in accordance with step (b).

The particulate pigment utilized in step (a) of the above process is preferably pigment which has not been milled or micronized. The preferred non-treated titanium dioxide pigment for use in the process of this invention can be of either the anatase or rutile crystalline structure or a combination thereof. The titanium dioxide pigment can be produced by a commercial process which is well known to those skilled in the art such as the sulfate process or the vapor phase chloride oxidation process.

The surface active agents which can be utilized in accordance with the present invention include alkyl alcohols ethoxylated with from 4 to 14 ethylene oxide groups and wherein the alkyl groups have from 6 to 16 carbon atoms, ethoxylated sorbitan derivatives having hydrophile-lipophile balances (HLB values) in the range of from 1 to 20, a mixture of non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides having HLB values in the range of from 1 to 20 and mixtures of said ethoxylated sorbitan derivatives, said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides.

Of the foregoing surface active agents, a mixture of ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15, non-ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 and ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 is preferred. The ethoxylated sorbitan derivatives are preferably present in the mixture in an amount in the range of from 5 percent to 100 percent by weight of the mixture with the non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides making up

the remainder of the mixture. A more preferred mixture of the ethoxylated sorbitan derivatives, non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides contain the ethoxylated sorbitan derivatives in an amount in the range of from 15 percent to about 70 percent by weight of the mixture with the non-ethoxylated and ethoxylated mono and diglycerides making up the remainder of the mixture. Most preferably, the surface active agent mixture contains the ethoxylated sorbitan derivatives in an amount of about 70 percent with non-ethoxylated and ethoxylated mono and diglycerides making up the remaining 30 percent by weight of the mixture.

An example of a suitable commercially available ethoxylated sorbitan derivative which can be utilized in accordance with this invention is an ethoxylated sorbitan monooleate sold by BASF Corporation under the trade designation "T-MAZ-81™." An example of a suitable commercially available mixture of non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides which can be utilized is sold by Loders Croklaah Company under the trade designation "Tally 100 Plus™."

The slurry formed in step (a) described above contains pigment in an amount in the range of from 10 to 50 percent by weight of the slurry, preferably an amount in the range of from 20 to 40 percent and most preferably about 34 percent by weight. The slurry is formed in accordance with step (a) at a temperature in the range of from 10°C to 90°C, preferably from 15°C to 80°C and most preferably at a temperature of 25°C.

The pH of the slurry formed in step (a) is adjusted, if necessary, to a pH in the range of from 7.0 to 13.0, more preferably a pH of from 8.0 to 11.0 and most preferably about 9.5. Also, the slurry can optionally be filtered to increase the pigment content of the slurry to in the range of from 40 to 95 percent solids prior to carrying out step (b).

The process of the present invention can also optionally include the step of coating the pigment with a metal oxide while the pigment is in the slurry formed in step (a). Examples of metal oxides which can be used include, but are not limited to, aluminum oxide, silica and zirconium oxide. Preferably, the coating of the pigment with a metal oxide yields a coating of from 0.25 to 1.5 percent metal oxide by weight of pigment. Such coatings improve the pigmentary properties of the pigment product and are well known to those skilled in the art.

The surface active agent utilized is preferably mixed with the slurry in accordance with step (b) in an amount in the range of from 0.1 to 5.0 percent by weight

of pigment in the slurry, more preferably in an amount in the range of from 0.25 to 2.0 percent and most preferably in an amount of 1.0 percent. The mixing of the surface active agent with the slurry in accordance with step (b) is preferably carried out in a time period in the range of from 5 minutes to 24 hours, preferably in a time period from 5 minutes to 30 minutes and most preferably in a time period of about 5 minutes.

The surface active agent is preferably coated on the pigment in accordance with step (b) in an amount in the range of from 0.1 to 5 percent by weight of the pigment, more preferably in an amount of from 0.5 to 2 percent by weight and most preferably in an amount of about 1 percent by weight of the pigment.

The drying of the surface active agent coated pigment in accordance with step (c) is preferably carried out by spray drying the pigment. However, as will be understood by those skilled in the art, other drying equipment can be utilized such as an agglomerator, a fluid bed dryer or the like. As mentioned above, if desired, the dried coated pigment can be micronized.

A preferred process of the present invention for preparing an improved titanium dioxide pigment which is more readily dispersible in paints and plastics concentrates than prior art pigments comprises the following steps: (a) mixing a particulate titanium dioxide pigment with water to form a slurry of the pigment and water; (b) mixing a surface active agent with the slurry of step (a) so that the pigment is coated therewith, the surface active agent being a mixture of ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15, non-ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 and ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15; and (c) spray drying the titanium dioxide pigment coated in accordance with step (b).

The ethoxylated sorbitan derivative in the mixture of surface active agents is preferably present therein in an amount of 70 percent by weight of the mixture with the non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides making up the remainder of the mixture. Also, the pigment is preferably present in the slurry formed in step (a) in an amount of about 34 percent by weight of the slurry and the slurry is preferably formed at a temperature of about 25°C. The surface active agent mixture is mixed with the slurry in accordance with step (b) in an amount of about 1 percent by weight of pigment in the slurry, and the surface active agent is preferably

coated on the pigment in accordance with step (b) in an amount of about 1 percent by weight of the pigment. Step (c) is preferably carried out in a time period of about 5 minutes. When the pigment is coated with a metal oxide during step (a), if necessary, the pH of the slurry can be adjusted to in the range of from 8 to 11. Also, as mentioned
5 above, the slurry can be filtered to increase the concentration of pigment in the slurry prior to carrying out step (b).

Another process of this invention for preparing improved pigment which is more readily dispersible in paints and plastics concentrates is comprised of the following steps: (a) mixing a non-micronized particulate pigment with water to form a
10 slurry of the pigment and water; (b) milling the slurry formed in step (a) to produce an average pigment particle size therein in the range of from 0.1 microns to about 1 micron; (c) mixing a surface active agent with the slurry of step (b) so that the pigment is coated therewith; and (d) drying the pigment coated in accordance with step (c). As mentioned, the dried pigment can be micronized if desired.

15 The surface active agents which can be utilized in the immediately preceding process for preparing pigment are the same as those described above. Also, the slurry formed in step (a) contains pigment in the amounts set forth above and has a temperature in the range described above.

The milling of the slurry in step (b) is carried out to produce an average pigment
20 particle size in the slurry in the range of from 0.1 microns to 1 micron, preferably a size in the range of from 0.1 microns to 0.8 microns and most preferably, an average particle size of about 0.2 microns and with substantially all of the particles being about 0.6 microns or less in diameter as demonstrated in the Examples below. While a variety of milling apparatus can be utilized, a sand mill is preferred.

25 After the slurry is milled, and as mentioned above, the pH of the slurry can be adjusted to the levels described above and can be filtered as described above. Further, the pigment in the milled slurry can be coated with a metal oxide in the amounts described above.

30 The surface active agent utilized is mixed with the slurry in accordance with step (c) in the amounts given above, the mixing of the surface active agent with the slurry is carried out in the time mentioned above and the surface active agent is coated on the pigment in the amounts given above. Finally, the drying of the surface active

agent coated pigment in accordance with step (d) is preferably carried out by spray drying the pigment but other drying equipment can be utilized. If the dried product produced in step (d) is subsequently micronized, a jet mill is preferably utilized.

5 A preferred process of the present invention for preparing an improved titanium dioxide pigment which is dispersible in paints and plastics concentrates comprises the following steps: (a) mixing a non-micronized particulate titanium dioxide pigment with water to form a slurry of the pigment and water; (b) milling the slurry formed in step (a) to produce an average pigment particle size therein in the range of from 0.1
10 microns to 1.0 micron; (c) mixing a surface active agent with the slurry of step (b) so that the pigment is coated therewith, the surface active agent being a mixture of ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15, non-ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 and ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15; and (d) spray drying the titanium dioxide pigment coated in accordance with step (c).

15 The ethoxylated sorbitan derivative in the mixture of surface active agents is preferably present therein in an amount of about 70 percent by weight of the mixture with the non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides making up the remainder of the mixture. Also, the pigment is preferably present in the slurry formed in step (a) in an amount of about 34 percent by weight of
20 the slurry, and the slurry is preferably formed at a temperature of about 25°C. The surface active agent mixture is mixed with the slurry in accordance with step (c) in an amount of about 1 percent by weight of pigment in the slurry, and the surface active agent is preferably coated on the pigment in accordance with step (c) in an amount of about 1 percent by weight of the pigment. Also, step (c) is preferably carried out in a
25 time period of about 5 minutes. The dried titanium dioxide pigment produced in step (d) can be micronized if desired, preferably by jet milling.

As mentioned above, if desired, the pigment can be coated with a metal oxide during step (b), and, if necessary, the pH of the slurry can be adjusted to in the range of from 8 to 11. Also, as mentioned above, the slurry can be filtered to increase the
30 concentration of pigment in the slurry prior to carrying out step (c).

The dispersible pigments of this invention are particularly suitable for use in the preparation of paints and plastics concentrates. In preparing the paints and plastics

concentrates, the pigment is incorporated into the paints or plastics in an amount which varies depending upon the level of pigmentation required in the final or finished end product. Generally, the paints and plastics concentrates can contain weight ratios of the pigment of this invention to the paints or plastics in which they are dispersed in the range of from 0.5:1 to 5:1. Within the above range, the pigment of this invention can be easily and uniformly dispersed or distributed throughout the paint or plastic.

In order to further illustrate the process of the present invention, the following examples are given.

Example 1

A titanium dioxide, chloride grade, burner discharge pigment was dispersed in water at 34 percent by weight pigment and sandmilled until 97 percent of the pigment particles were less than 0.63 microns in diameter as measured by a conventional particle size analyzer. The slurry was pressure filtered in the presence of a cationic flocculant. The resulting filter cake was redispersed in water containing a mixture of 70 percent commercially available ethoxylated sorbitan monooleate (T-Maz-81) and 30 percent of a commercially available mixture of non-ethoxylated and ethoxylated mono and diglycerides (Tally 100 Plus), the mixture being present in the water in an amount of 1 percent by weight of the pigment dispersed therein. Water was added to the slurry until the rheological characteristics of the slurry allowed pumping and feeding to a spray drier. The finished pigment had a tap density of 1.7 and an aerated density of 0.9. The equilibrium torque for the finished pigment as measured by a Brabender torque rheometer instrument was 1166 meter-grams in a low density polyethylene with a pigment loading of 75 percent by weight. By comparison, two dusty and poor flowing commercial titanium dioxide pigments had equilibrium torque values of 1220 and 1270 in the same test.

Example 2

The same pigment procedures and additives as in Example 1 were used except that the pigment was sandmilled until 97 percent of the particles were less than 0.63 microns in diameter. The chloride grade burner discharge titanium dioxide pigment was dispersed in water at 34 percent by weight pigment and sandmilled. The slurry was pressure filtered and the filter cake was redispersed in water containing a mixture

of the surface active agents described in Example 1, in an amount of 1 percent by weight of the pigment dispersed therein. Water was added to the slurry until the rheological characteristics of the slurry allowed pumping and feeding to a spray drier. The spray drier discharge was micronized and had an equilibrium torque as measured
5 by a Brabender instrument of 1103 meter-grams in polyethylene with a pigment loading of 75 percent by weight. By comparison, two dusty and poor flowing, commercially-available titanium dioxide pigments had equilibrium torque values of 1220 and 1270 in the same test.

Example 3

10 The same chloride grade, burner discharge titanium dioxide pigment was dispersed in water at 34 percent by weight pigment and sandmilled until 90 percent of the particles were less than 0.63 microns in diameter. The slurry was pressure filtered and the filter cake was redispersed in water containing a 1 percent by weight mixture of the surface active agents described in Example 1. Water was added to the slurry until
15 the rheological characteristics of the slurry allowed pumping and feeding to a spray drier. The equilibrium torque for the finished pigment as measured by a Brabender instrument was 1254 meter-grams in polyethylene with a pigment loading of 75 percent by weight. Two dusty and poor flowing, commercially-available titanium dioxide pigments presently sold in the commercial market by others had equilibrium torque
20 values of 1220 and 1270 in the same test.

Example 4

Chloride grade, burner discharge titanium dioxide pigment was dispersed in water at 34 percent by weight pigment and sandmilled until 90 percent of the particles were less than 0.63 microns in diameter. The slurry was pressure filtered and the filter
25 cake was redispersed in water containing a 1 percent by weight mixture of the surface active agents described in Example 1. Water was added to the slurry until the rheological characteristics of the slurry allowed pumping and feeding to the spray drier. The finished pigment had a tap density of 1.7 and an aerated density of 0.9. The equilibrium torque for the finished pigment as measured by a Brabender instrument was
30 1299 meter-grams in polyethylene with a pigment loading of 75 percent by weight. Two dusty and poor flowing, commercially-available titanium dioxide pigments had equilibrium torque values of 1220 and 1270 in the same test.

Example 5

Chloride grade, burner discharge titanium dioxide was dispersed in water at 34 percent by weight pigment and sandmilled until 97 percent of the particles were less than 0.63 microns in diameter. The slurry was then processed so that silica and alumina were deposited on the surface. A mixture of the surface active agents of this invention described in Example 1 was added to the slurry in an amount of 1 percent by weight of the pigment therein. Water was then added to the slurry until the rheological characteristics of the slurry allowed pumping and feeding to a spray drier. The resulting spray dried pigment was then micronized by jet milling.

The finished pigment of this invention was evaluated for dispersion in an alkyd resin paint formulation. In the evaluation, the dispersion of the pigment of the present invention prepared as described above after being added to an alkyd paint formulation and stirred at a constant rate was compared to the dispersion of two commercial titanium dioxide pigments in the same paint formulation and under the same conditions. The two commercial pigments were sold by others for use in alkyd resin paint formulations.

The dispersions of the three pigments were measured by a Hegman gauge. As the pigment particles being tested become more dispersed and less agglomerated in the alkyd resin paint formulation, the Hegman gauge indicated a higher value. The results of the tests are shown in the table below wherein "Pigment A" is the treated pigment of the present invention and "Pigment B" and "Pigment C" are the two commercial pigments.

TABLE

Time After Pigment Added, min.	Hegman Gauge Value		
	Pigment A	Pigment B	Pigment C
5	8	0.5	0
10	8	2.5	0
15	8	5	0
20	8	5.5	0
25	8	6.5	0.5
30	8	7.5	1
35	8	8	2

5 As can be seen from the Table, the treated pigment of this invention was completely dispersed in 5 minutes. Pigment B was not completely dispersed until being stirred for about 35 minutes and Pigment C was only beginning to disperse after 35 minutes.

1. A process for preparing an improved pigment which is dispersible in paints and plastics concentrates comprising the steps of:

5 (a) mixing a particulate pigment with water to form a slurry of the pigment and water;

(b) mixing a surface active agent with said slurry of step (a) so that said pigment is coated therewith, said surface active agent being selected from the group consisting of alkyl alcohols ethoxylated with from 4 to 14 ethylene oxide groups and wherein the alkyl groups have from 6 to 16 carbon atoms, ethoxylated sorbitan derivatives having HLB values in the range of from 1 to 20, a mixture of non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides having HLB values in the range of from 1 to 20 and mixtures of said ethoxylated sorbitan derivatives, said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides; and

15 (c) drying said pigment coated in accordance with step (b).

2. The process of claim 1 wherein said surface active agent is a mixture of ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15, non-ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 and ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15.

3. The process of claim 2 wherein said ethoxylated sorbitan derivatives form at least 5 percent by weight of said mixture, with said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides making up any remainder of said mixture.

4. The process of claim 1 wherein said surface active agent is entirely comprised of one or more ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15.

5. The process of any of claims 1 through 4, wherein said pigment is titanium dioxide.

6. The process of any of claims 1 through 5, wherein said slurry formed in step (a) contains pigment in an amount in the range of from about 10 percent to about 50 percent by weight of said slurry.

5 7. The process of any of claims 1 through 6 wherein said slurry formed in step (a) is at a temperature in the range of from 10° to 90°C.

8. The process of any of claims 1 through 7 wherein said surface active agent is mixed with said slurry in accordance with step (b) in an amount in the range of
10 from 0.1 percent to 5 percent by weight of pigment in said slurry.

9. The process of claim 1 which further comprises micronizing said dried pigment.

15 10. A process for preparing an improved low dusting, free-flowing, pigment which is dispersible in paints and plastics concentrates comprising the steps of:

(a) mixing a non-micronized particulate pigment with water to form a slurry of the pigment and water;

20 (b) milling the slurry formed in step (a) to produce an average pigment particle size therein in the range of from 0.1 microns to 1 micron;

(c) mixing a surface active agent with said slurry of step (b) so that said pigment is coated therewith, said surface active agent being selected from the group consisting of alkyl alcohols ethoxylated with from 4 to 14 ethylene oxide groups and wherein the alkyl groups have from 6 to 16 carbon atoms, ethoxylated sorbitan derivatives having HLB values in the range of from 1 to 20, a mixture of non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides having HLB
25 values in the range of from 1 to 20 and mixtures of said ethoxylated sorbitan derivatives, said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides; and

30 (d) drying said pigment coated in accordance with step (c).

11. The process of claim 10 wherein said surface active agent is a mixture of ethoxylated sorbitan derivatives having HLB values in the range of from 2 to 15, non-ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15 and ethoxylated mono and diglycerides having HLB values in the range of from 2 to 15.

12. The process of claim 10 or of claim 11, wherein said ethoxylated sorbitan derivatives form at least 5 percent by weight of said mixture, with said non-ethoxylated mono and diglycerides and said ethoxylated mono and diglycerides making up any remainder.

13. The process of claim 12 wherein said ethoxylated sorbitan derivatives are present in an amount of at least 70 percent by weight of said mixture .

14. The process of any of claims 10 through 13, wherein said milling in accordance with step (b) is carried out in a sand mill.

15. The process of any of claims 10 through 14 wherein said surface active agent is mixed with said slurry in accordance with step (c) in an amount of about 1 percent by weight of pigment in said slurry.

16. The process of any of claims 10 through 15 wherein said dried pigment produced in accordance with step (d) is subsequently micronized by jet milling.

17. The process of any of claims 10 through 16 wherein said pigment is titanium dioxide pigment.

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Published:

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For two-letter codes and other abbreviations, refer to the "Guidance Notes on Codes and Abbreviations" appearing at the beginning of each regular issue of the PCT Gazette.

(54) Title: PROCESS FOR PREPARING PIGMENTS DISPERSIBLE IN PAINTS AND PLASTICS CONCENTRATES

(57) Abstract: A process for preparing an improved pigment which is readily dispersible in paints and plastics concentrates is provided. In accordance with the process, a particulate pigment is mixed with water to form a slurry thereof, and a surface active agent is mixed with the slurry so that the pigment therein is coated therewith. A preferred surface active agent is a mixture of ethoxylated sorbitan derivatives, non-ethoxylated mono and diglycerides and ethoxylated mono and diglycerides. After the pigment has been coated with the surface active agent, the coated pigment is dried.



WO 02/059218 A3

INTERNATIONAL SEARCH REPORT

International application No.

PCT/US 02/01341

A. CLASSIFICATION OF SUBJECT MATTER

IPC7: C09C 3/08, C09C 1/36, C08K 9/04, C09D 7/12
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC7: C09C, C08K, C09D

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

EPO-INTERNAL, WPI DATA

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	US 5908498 A (JAMES W. KAUFFMAN ET AL), 1 June 1999 (01.06.99) --	1-17
A	US 5733365 A (JOHN E. HALKO ET AL), 31 March 1998 (31.03.98) -- -----	1-17

☐ Further documents are listed in the continuation of Box C.☒ See patent family annex.

* Special categories of cited documents:

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25 Sept 2002

Date of mailing of the international search report

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INTERNATIONAL SEARCH REPORT

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